



IED RELATING TO OIL AND GAS BURNERS FOR INDUSTRIAL USE

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**JOINT MEETING OF THE COAL RESEARCH FORUM, (CRF), ENVIRONMENT DIVISION, THE
COMBUSTION ENGINEERING ASSOCIATION, (CEA) AND THE ROYAL SOCIETY OF CHEMISTRY
ENERGY SECTOR, (RSC-ES)**

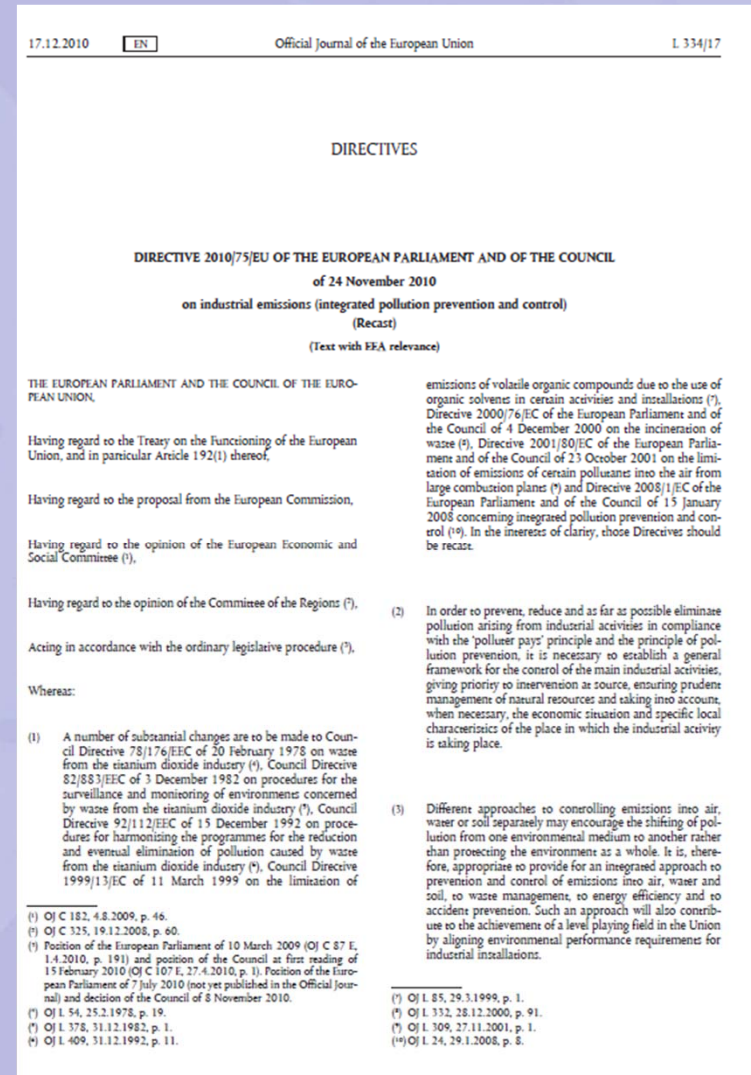
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EU Directive 2010/75/EU

- EU Directive 2010/75/EU of 24th November, 2010
- Industrial Emissions Directive (IED)
- Integrated Pollution Prevention and Control (IPPC)
- Member States transpose into National Laws



Combination of Existing Directives into IED

- Large Combustion Plant directive (LCPD);
- Integrated Pollution Prevention and Control directive (IPPCD)
- Waste Incineration directive (WID)
- Solvent Emissions directive (SED)
- Other directives relating to Titanium dioxide

UK Timetable

- Transposition into UK law by 6 January 2013
- New plant compliance from 6 January 2013
- Existing installations (but not existing LCP) comply by 6 January 2014
- Other activities not currently part of IPPC comply by 6 July 2015
- Existing LCP compliance from 1 January 2016

Large Combustion Plant – NOx Emissions

Emission Limits - Oil Firing			
NOx in mg/Nm ³ (corrected for dry gas at 3% oxygen)			
Thermal Input		New Plant	Existing Plant
50-100 MW		300	450
100-300 MW		150	200
>500 MW		100	150

Emission Limits - Gas Firing			
NOx in mg/Nm ³ (corrected for dry gas at 3% oxygen)			
Fuel		New Plant	Existing Plant
Natural Gas		100	100
Other (includes COG and BFG)		100	200

Large Combustion Plant – Dust and CO Emissions

Particulate (dust) and CO emissions apply equally to new and existing plant

Emission Limits - Oil Firing		
dust in mg/Nm ³ (corrected for dry gas at 3% oxygen)		
Thermal Input	dust	
50-100 MW	30	
100-300 MW	25	
>500 MW	20	

Emission Limits - Gas Firing		
dust and CO in mg/Nm ³ (corrected for dry gas at 3% oxygen)		
Fuel	dust	CO
General	5	100
BFG	10	
Steel Industry Gas	30	

Large Combustion Plant – SO₂ Emissions

SO₂ emissions apply equally to new and existing plant

Emission Limits - Oil Firing			
SO ₂ in mg/Nm ³ (corrected for dry gas at 3% oxygen)			
Thermal Input		SO ₂	
50-100 MW		200	
100-300 MW		200	
>500 MW		150	

Emission Limits - Gas Firing			
SO ₂ in mg/Nm ³ (corrected for dry gas at 3% oxygen)			
Fuel		SO ₂	
General		35	
LPG		5	
COG		400	
BFG		200	

What Can Be Achieved?

Typical Burners for Fire Tube Boilers
Individual Burners up to 25 MW

Achievable Emissions – Package Burners

Emissions in mg/Nm³
(corrected for dry gas at 3% oxygen)

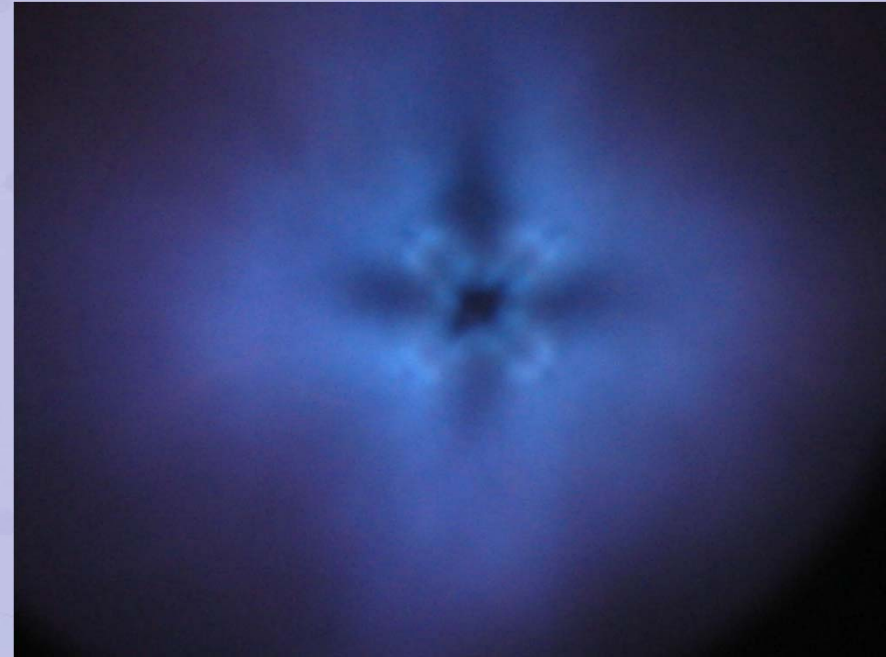
Fuel	NOx	CO	SO ₂	dust
Natural Gas	<80	<5	n/a	<5
Lpg	<200	<5	n/a	<5
Gas Oil	<180	<50	n/a	<20
HFO	<550	<100	1700 per 1% in fuel	<150

Above emissions are achievable without
post-combustion cleaning systems, i.e.
based on low NOx burner technology only



Packaged Burners for Fire Tube Boilers

- Gas, Oil and Dual Fuel Burner
Sizes from 3 to 25 MW
- NO_x reduction through air
and/or fuel staging
- Low CO across turn-down
range
- Wide turn-down range 6:1 or
greater
- Excessive SO₂ and dust
emissions only from HFO
combustion – depend on fuel
composition
- HFO NO_x is higher due to N in
fuel



What can be Achieved?

Typical Burners for Water Tube Boilers

Individual or Multi-Burner Installations

Burner Sizes from 3 to 100 MW

Multi-Burner Boilers up to 600 MW

Achievable Emissions – Power Burners

Emissions in mg/Nm³

(corrected for dry gas at 3% oxygen)

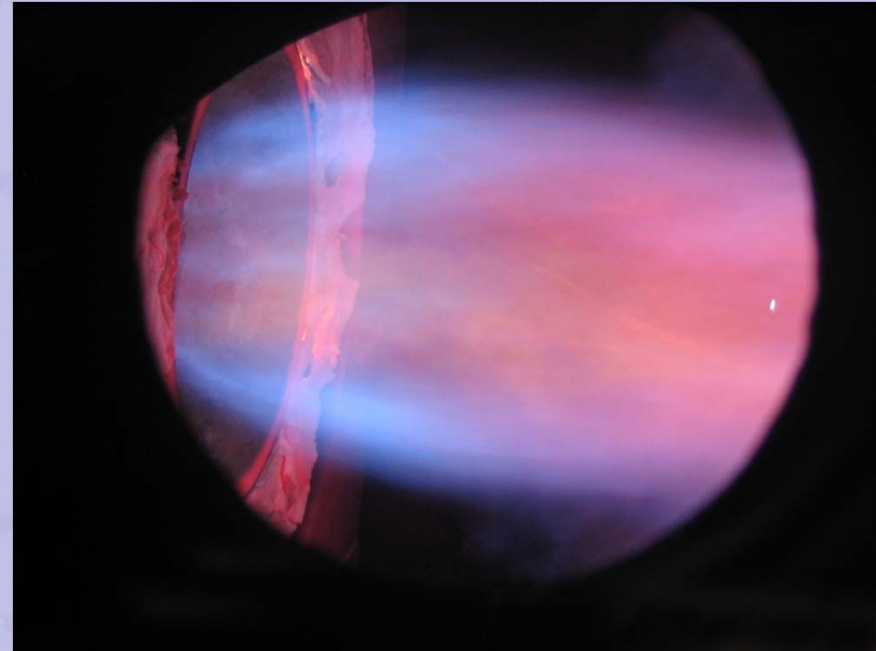
Fuel	NO _x	CO	SO ₂	dust
Natural Gas	<100	<5	n/a	<5
Lpg	<100	<5	n/a	<5
Gas Oil	<100	<50	n/a	<20
HFO	<350	<100	1700 per 1% in fuel	<100

Above emissions are achievable without
post-combustion cleaning systems i.e.
based on low NO_x burner technology only



Power Burners for Water Tube Boilers

- Gas, Oil and Dual Fuel Burner
Sizes from 3 to 100 MW
- NO_x reduction through air and/or fuel staging. BAT is less than 20 mg/Nm³ of NO_x gas firing
- Low CO across turn-down range
- Wide turn-down range 6:1 or greater
- Excessive SO₂ and dust emissions only from HFO combustion – depends on fuel composition
- NO_x from HFO depends on fuel nitrogen but can be less than 350 mg/Nm³ with low NO_x burner technology



Factors Affecting Burner NOx Emissions

- Excess air
- Air Preheat
- Firing Intensity
 - Heat Release per Furnace Volume
- Turbulence and Mixing
- Fuel Composition

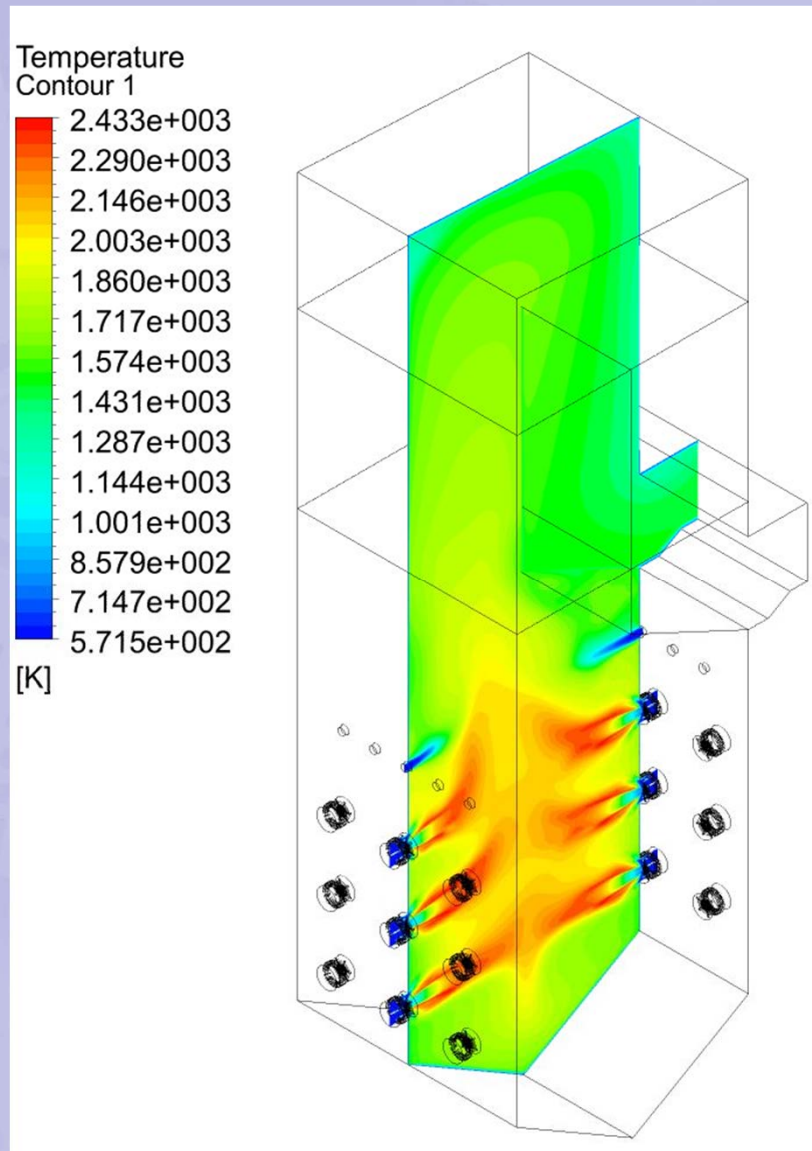
Post Combustion Emissions Reduction

- Costly systems applicable mainly for larger plant i.e. high pressure steam boilers
- In-furnace NO_x reduction
- Flue Gas Acid Gas Scrubbing
- Dust Removal Systems

In-Furnace Systems

- Flue Gas Recirculation (FGR)
 - NO_x reduction up to 75%
 - Some burners can use 30% or more FGR
 - Additional or larger fan required – increased electricity use
 - Increases mass flow
- Water Injection through Burner
 - NO_x reduction up to 20%
 - Increases mass flow
 - Reduces efficiency
- Steam injection in (Gaseous) Fuel
 - NO_x reduction up to 40%
 - Can use low pressure 'waste' steam
 - up to 0.5 kg / kg of fuel
- Steam injection in Air
 - NO_x reduction up to 25 %

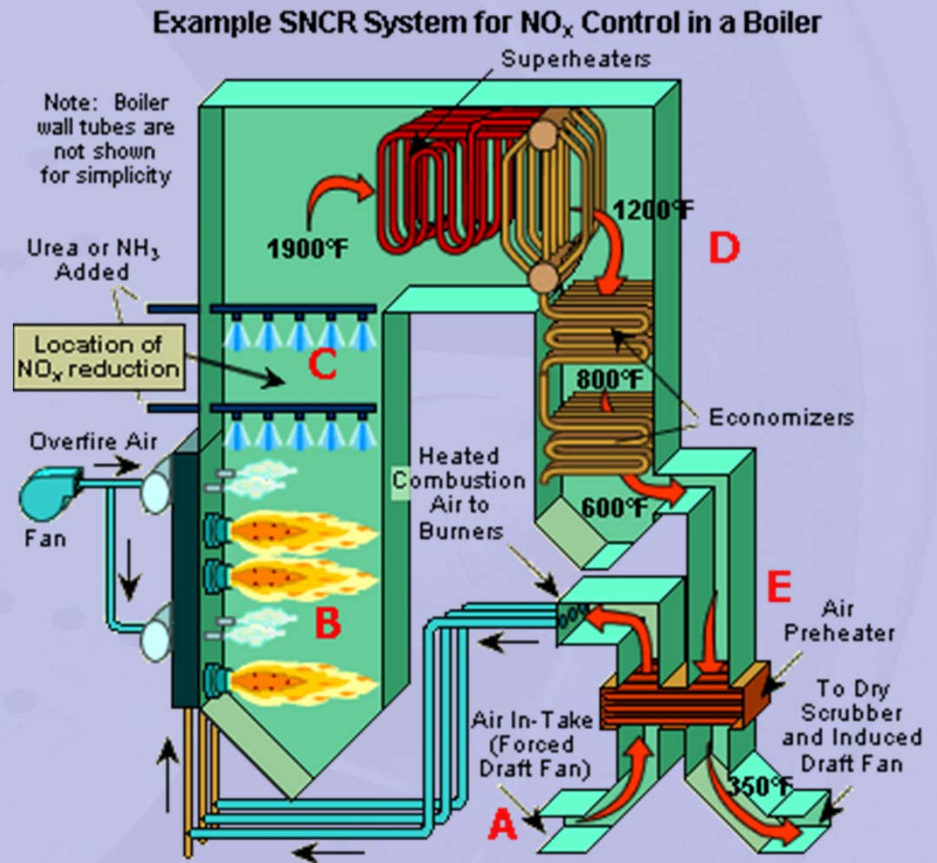
In-Furnace Systems, *Continued*



- Over-fire Air (OFA) or After Burner Air (AAP)
 - Applicable for multi-burner systems
 - Air Ports above top row of burners
 - Burners operate sub-stoichiometrically
 - Use CFD to aid design
 - NOx reduction up to 40%
- Row Staging
 - Lower Burners operate sub-stoichiometrically
 - Higher burners operate with higher excess air
 - NOx reduction up to 10%

In-Furnace Systems, *Continued*

- Selective Non-Catalytic Reduction (SNCR)
 - In-furnace injection of ammonia or urea
 - Limited temperature window (900 to 1000 °C)
 - Not suitable for all applications
 - NO_x reduction 40 to 80%
 - Risk of ammonia 'slip'
 - Ammonia emission limit <5 mg/Nm³
- Re-burn
 - Similar to OFA but with additional gas burning downstream in furnace



Post Combustion Gas Cleaning

- SO₂ Removal
 - Wet scrubbing
 - Packed bed or venturi
 - Dry scrubbing
 - Lime injection in bag house
 - Efficiency >95% is possible
- Dust Removal
 - Bag House
 - ESP
 - Efficiency > 95% is possible



Post Combustion Gas Cleaning

NOX Reduction

- Selective Catalytic Reduction (SCR)
 - Injection of ammonia or urea
 - Catalyst bed to achieve efficiency
 - Capable of operating at low temperature
 - Suitable for installation after boiler and heat recovery
 - NOx reduction >90%
 - Ammonia emission limit <5 mg/Nm³

Terms and Conditions

- For retrofit applications, specific limits may not always be achievable due to furnace shape and firing intensity
- SO₂ and particulate emissions depend on fuel composition
- 1% S → 1700 mg/Nm³ of SO₂
- Ash in fuel is unchanged by combustion process

How Can NOx Limits Be Achieved?

Emission Limits - Oil Firing

NOx in mg/Nm³

(corrected for dry gas at 3% oxygen)

Thermal Input	New Plant	Existing Plant	
50-100 MW	300	450	Can be achieved on some fire-tube boilers with gas oil and HFO firing and in-furnace techniques
100-300 MW	150	200) Requires SNCR or SCR systems for HFO
>500 MW	100	150) combustion, low NOx burner technology for gas) oil combustion

Emission Limits - Gas Firing

NOx in mg/Nm³

(corrected for dry gas at 3% oxygen)

Fuel	New Plant	Existing Plant	
Natural Gas	100	100) Achievable with low NOx burner technology in all
Other (includes COG and BFG)	100	200) applications)

Summary

- Gas Firing Emission limits can generally be achieved with low NOx burner technology only - for most commercially available fuels
- Where fuels contain sulphur, ash or nitrogen (e.g. HFO) post combustion gas cleaning systems are almost certainly required
- Oil firing NOx emissions can generally be achieved with a combination of low NOx technology and in-furnace techniques
- Consideration of furnace and burner design together for new installations will be important for minimisation of emissions